## AMENDMENTS TO THE CLAIMS

ì

- (currently amended) A process for preparing ethylene polymers carried out in the presence
  of a catalyst system comprising (i) a solid catalyst component comprising Mg, Ti, halogen,
  and optionally an internal electron donor compound (ID), and (ii) an Al-alkyl compound;
  said process comprising at least two stepsteps of polymerization (a) and (b), in which:
  - in a first step (a) ethylene is polymerized in the presence of a molecular weight regulator in order to produce an ethylene (co)polymer; and
  - in a further step (b), which is carried out in the presence of an external electron donor compound (OD) added to this polymerization step as a fresh reactant, ethylene is copolymerized with an alpha olefin comonomer of formula CH<sub>2</sub>=CHR, in which R is a C1-C20 hydrocarbon group, to produce an ethylene copolymer having a molecular weight higher than that of the ethylene (co)polymer produced in step (a).
- 2. (original) The process according to claim 1 in which the solid catalyst component (i) comprises a Ti compound and a magnesium dihalide.
- 3. (currently amended) The process according to claim 2 in which the solid catalyst component (i) further comprises an <u>internal</u> electron donor compound (ID) selected from alcohol, glycols, esters, ketones, amines, amides, nitriles, alkoxysilanes and ethers.
- 4. (currently amended) The process according to claim 3 in which the <u>internal</u> electron donor compound (ID) is tetrahydrofurane or ethylacetate.
- 5. (currently amended) The process according to claim 1 in which the <u>outsideexternal</u> electron donor compound (OD) added to the polymerization step (b) as a fresh reactant is THF.
- 6. (original) The process according to claim 1 which is carried out in gas-phase.
- 7. (currently amended) The process of claim 6 in which the polymerization stepsteps (a) and(b) are carried out in two fluidized bed reactors.
- 8. (currently amended) The process of claim 6 in which the polymerization step (a) is <u>carried</u> out in a fluidized bed reactor, and the step (b) is carried out in a gas-phase reactor having two interconnected polymerization zones.
- 9. (original) The process according to claim 1 in which the polymerization step (a) is carried out in the presence of hydrogen.

- 10. (currently amended) The process according to claim 1 in which the <u>alpha-olefin</u> comonomer used in polymerization step (b) is selected from 1-butene, 1-pentene, 1-hexene, 4-methyl-1-pentene, 1-heptene and 1-octene.
- 11. (currently amended) The process according to claim 1 in which the alkyl-Al compound (ii) is selected from the trialkyl aluminum compounds.
- 12. (original) The process according to claim 11 in which the trialkyl aluminum compound is used in mixture with alkylaluminum halides.
- 13. (currently amended) The process according to claim 1 in which the components (i), (ii), and optionally the <u>external electron donor compound</u> (OD) <del>compound</del> are pre-contacted before being introduced into thea reactor, for a period of time ranging from 0.1 to 120 minutes at a temperature ranging from 0 to 90°C.
- 14. (currently amended) The process according the claim 1 in which in the polymerization step (a) is produced an ethylene polymer having a density not less than 0.955 kg/dm<sup>3</sup> and in the copolymerization step (b) the copolymer produced has an average molecular weight ranging from 100000 to 1.000.0001,000,000 g/mol.